

Application of Nanofluids for Cooling Newtonian and Non-newtonian Blood Mimicking Fluids Flow in Annular Space

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Abstract: An experimental study performed to investigate the effect of nanofluid forced convection heat transfer and fluid flow characteristic. Three types of nanofluids $\{\gamma\text{Al}_2\text{O}_3, \text{CuO}$ and $\text{ZrO}_2\text{-DIW}\}$ flow under laminar or turbulent condition in inner pipe. The shear thinning behavior of blood is more accurately modeled by non-Newtonian Blood Mimic Fluids BMF. Here heat transfer and friction factor correlations developed for nonreactive Newtonian and non-Newtonian BMF fluids of (water: glycerol: xanthan gums) and heparinized bovine blood. The results show that the BMF Nusselt number (Nu_b) increased as increasing Graetz number, and as flow index (n) decreasing. Bovine blood gives the temperatures distribution similar to (BMF6) but with lower Nusselt number by (31.2%). The BMF friction factor increases with decreasing (n), but the Bovine blood gives higher friction factor as compared with BMF6 by (25.6%). It was observed that all nanofluids types showed higher heat transfer characteristics than the base fluid DIW. It was also noted that in the $\gamma\text{Al}_2\text{O}_3$ shows higher enhancement than the other by (82.4%) at ($\text{Re}_{\text{nf}}=12670$) and ($\phi=1 \text{ vol.}\%$). Comparisons present experimental results with previously reported results it gives good agreement.

Keywords: Non-newtonian Fluids, Nanofluids, Hypothermia, Intravenous Cooling

1. Introduction

The heat transfer characteristics in blood heat exchangers BHE used in many medical applications for cooling biofluid such as blood, where recently the most effective hypothermia method used is intravenous cooling catheters inserted in the vena cava blood vessel (IVC) and by using water as the usual cooling or warming medium. The non-Newtonian blood flows in annular space between the blood vessel wall and cooling catheter studied by [1, 2]. Convective heat transfer in double pipe systems can be enhanced in several ways, by using either active or passive techniques. The active case, is to modify the fluid itself by enhancing its thermal conductivity. Various techniques have been used to increase the thermal conductivity of base fluids by introducing solid particles whose conductivity is generally higher than that of liquids. New classes of fluids called Nanofluids have recently been developed, tested and studied by Sebastien et al. [3], Choi [4], Zeinali et al. [5], Anoop et al. [6] and Zhang et al. [7]. Byung et. al. [8] Aghayari et. al., [9], Sudarmadji, [10],

Mohamed et. al., [11] performed an investigation for the convective heat transfer coefficient of nanofluids made of several alumina nanoparticles and transformer oil flowing through a double pipe heat exchanger system in laminar nanofluids exhibited a considerable increase of heat transfer coefficients of alumina is much higher than that of the base fluids. Masoud et al. [12] studied the plate and concentric tube heat exchangers by using water-water and nanofluid-water streams. The ZnO/water (0.5 vol. %) nanofluid has been used as the hot stream. They results show that heat transfer rate and heat transfer coefficients of the nanofluid is higher than that of the (water). In the concentric heat exchanger the heat transfer coefficient of nanofluid at ($m=10\text{g/s}$) is about (14%) higher than the base fluid. Bozorgan et al. [13] used nanofluids as coolant candidate in chemical processes for water waste remediation. The inlet and outlet temperatures of hot solvent stream are equal to (40°C and 30°C), respectively. The flow rate of hot solvent stream is (0.8 kg s^{-1}). The inlet temperature of nanofluid coolant is equal to (5°C). Al_2O_3 nanoparticles dispersed in

water with volume concentrations up to (2 vol. %) were selected as a coolant. The results show that the flow rate of nanofluid coolant decreases with the increase of concentration of nanoparticles in the exchanger with a given heat exchange capacity.

The study of blood flow through an axisymmetric annular tube has been the subject of many studies, due to its relevance to blood flow in a catheterized artery studied by [14, 15, 16 and 17]. Dash et. al. [18] estimated the increased flow resistance in a narrow catheterized artery using the Casson fluid model. Banerjee et al. [19] investigated the changes in flow and mean pressure gradient across a coronary artery using power law and Carreau model, a shear-rate-dependent non-Newtonian fluid model. Jason [20] models two dimensional, axis-symmetric, counter flows with two domains of the catheter balloon and the vena cava blood vessel. Implemented in COMSOL program to modeling the intravenous catheter cooling system, Chose to model both the vessel and the catheter as concentric cylindrical tubes for simplicity sake. His results show that whether increasing the length of catheter and decreasing the cooling fluid temperature or decreasing the length of the catheter and increasing the cooling fluid temperature reduces the treatment time significantly. Laminar flow with pseudo-plastic and dilatant fluids (power-law models) was studied experimentally by [21, 22 and 23] studied the friction factors and heat transfer with power-law fluids with flow index of 0.5 to 1.0. They showed that the friction factor increased with decrease in the flow index and he Nusselt number increased with decreasing flow indices (n) and Nusselt number increases with decreasing (n). The flow of non-Newtonian fluid in annulus also studied by [24, 25]. Very little work has been done in the experimental study the flow and thermal characterizations together of BMF flows in annular space and cools by nanofluid flows in inner pipe in double-pipe heat exchanger. In this study using simulation of human blood flow in annulus between the cooling catheter wall (inner pipe) and the IVC blood vessel wall (outer pipe) of the intravascular cooling catheter, to find the temperature distribution around the catheter, using two domains of the BMF and the effect of using nanofluids instead of DIW with opposite direction flows.

2. Experimental Apparatus

(Figure. 1) shows the schematic diagram of experimental loop, it consists of a test section, a two centrifugal pump, condensation unit with immersion coil and a heating unit. The test section is a (1.0 m) long counter flow double-pipes heat exchanger with DIW flows inside the inner pipe while hot BMF flows in the annular space. The inner tube is made from a non-corrosive medical suitable smooth stainless steel (SS 304) with external diameters (10.05 mm) and (8.75 mm). The outer tube is made from transparent plastic diameters of (30.25 mm) and (23.45 mm). The test section is thermally isolated from its upstream and downstream section by rubber plug, and thermally isolated on the external surface of the

outer tube. Seven thermocouples are mounted at different longitudinal positions on the inner pipe surface. The inlet and exit temperatures of DIW and BMF are measured using four T-type thermocouples. Two receiver tanks of (20 L) are made from glass to store the BMF and nanofluids leaving the test section. The hot BMF flow rate are controlled by a flow meter (Model LD100, MLW, Germany) was used to initially adjust the desired flow rate in each experiment, but exact measurements were obtained by weighing fluid samples collected at determined time intervals. under the laminar condition only of (1-7 l/min), it calibrated to fit work with the non-Newtonian fluid flow, for nanofluid flow under laminar and turbulent conditions using flow meters of (0.3-0.8 l/min) and (1.8-18 l/min) respectively.

3. BMF Sample Preparation

In the preparation process of Newtonian (BMF1 and BMF2) models using fluids content the (water: Glycerin) mixture. By adding the DIW into (5 liters) beaker, and then add the glycerin liquid, the glycerin should try to settle down because it's high viscosity and density than the DIW. Water and glycerol are easily miscible so it will dilute easily and if they mixed gently with stirring they will miscible quickly using a mechanical agitation stirring for (20 min) until the solution is reaches the homogeneous state. But preparation process of non-Newtonian (BMF3 and BMF4) and (BMF5 and BMF6) models with a high rheological properties using two polymer types, the first consist of two BMF of (water: xanthan gum), the second BMF using include two BMF of (water: Glycerin: xanthan gum), where the ternary mixture water-glycerol-xanthan simulates the non-Newtonian rheological behavior of blood. was produced by filling the beaker of (5 liters) by specified weighted ratio of the DIW and adding the polymer powder lightly sprinkled into the water and stirring continued using the mechanical agitation stirring for about (one hour) to ensure completely polymer dissolution. The prepared BMF models was kept at rest at room temperature for (24 hr) prior to conducting the measurements of rheological parameters (m) and (n) by power law of ($\tau=m(\dot{\gamma})^n$) given by Brookfield DV-II+Pro coaxial rotational rheometer and using the Rheocalc software (version 3.2) for data acquisition and compared the parameters with [26, 27] and give good agreements. Thermophysical properties also measured and listed shows in (Table. 1). Also was used (3.0 liters) heparinized bovine blood with a hematocrit of (35%). The blood is mixed gently every (5 minutes) to keep it homogenous. In the beginning of the first experiment, the blood is re-circulated for one minute through the primary reservoir to ensure that all components of the system work properly without loss of blood.

4. Preparation of Nanofluid

Three types of nanoparticles of (Alumina Al_2O_3 , Copper Oxide CuO and Zirconia ZrO_2) are used in this research. All thermophysical properties for the three types of the

nanoparticle and the base fluid are given in (Table. 2). The Two-steps method is used for preparation of nanofluid. By using the electronic gram scale, to get the desired mass of nanopowder, the dispersant weighed powder (Al_2O_3 , CuO or ZrO_2) nanoparticles were dissolved in the DIW. The volume of mixture (water/nanoparticles) was set at (3.0 liters). This mixture was mixed slowly in the sonicator that can be timed for a maximum of (15-20 minutes) to break up any particle aggregates. All the suspensions, that had an ink-like

appearance, were stored at ambient temperature and checked periodically for visual changes. In this research during the experiments five volume concentrations (0.02, 0.06, 0.2, 0.6 and 1.0 vol. %) for (Al_2O_3 and CuO and ZrO_2). All thermophysical properties of these nanofluids employed are measured experimentally by using certificated instruments. (Figure. 2) show samples of (ZrO_2 -DIW, CuO-DIW, $\gamma\text{Al}_2\text{O}_3$ -DIW) nanofluids

Table 1. Thermophysical and rheological properties measurements of BMF and Bovine blood.

BMF Model	Rheological Relation	Flow Index (n)	Density ρ (g/m ³)	Specific heat C_p (J/kg K)	Thermal conductivity W/m. K
BMF1	$\tau=0.00286(\dot{\gamma})^n$	1.0	1.0321	3977.726	0.51586
BMF2	$\tau=0.00364(\dot{\gamma})^n$	1.0	1.0124	3967.116	0.51076
BMF3	$\tau=0.01726(\dot{\gamma})^n$	0.5643	0.5752	4244.126	0.53676
BMF4	$\tau=0.00241(\dot{\gamma})^n$	0.3977	0.4123	4308.306	0.57466
BMF5	$\tau=0.02514(\dot{\gamma})^n$	0.7921	0.8128	3305.726	0.52576
BMF6	$\tau=0.32612(\dot{\gamma})^n$	0.5134	0.5573	3472.216	0.54736
Bovine Blood	$\tau=0.26889(\dot{\gamma})^n$	0.6319	0.7472	3893.355	0.52214

Table 2. Nanoparticle and Base Fluid Properties.

Particle	ρ_p (kg/ m ³)	k_p (W/m. C)	cp_p (J/kg. C)	d_p (nm)	Color
$\gamma\text{Al}_2\text{O}_3$	3970	40	880	20	white
CuO	6500	13.5	535.6	40	black
ZrO_2	5680	2	418	80	white
Base fluid	ρ_f (kg/ m ³)	k_f (W/m. c)	cp_f (J/kg. c)	μ_f (nm)	
DIW	997.1	0.6017	4183	0.000957	

5. Data Reduction

5.1. BMF Calculations

The heat transfer coefficients and pressure drop of BMF can be calculated from the following equations:

The heat transfer rate into the BMF is defined as:

$$Q_b = \dot{m}_b C_{p_b} (t_{in} - t_{out})_b \quad (1)$$

The heat transfer rate into the DIW is defined as:

$$Q_{nf} = \dot{m}_{nf} C_{p_{nf}} (t_{out} - t_{in})_{nf} \quad (2)$$

The average heat transfer rate is defined as follows:

$$Q_{ave} = \frac{Q_b + Q_{nf}}{2} \quad (3)$$

The experimental local heat transfer coefficient and Nusselt number of the BMF are computed from the following equations.

The convection BMF heat flux can be represented by:

$$q_b = \frac{Q_b}{A_i} \quad (4)$$

where A_i is the heat transfer area given by:

$$A_i = \pi d_i L$$

The BMF local heat transfer coefficient can be obtained as:

$$\bar{h}_b = \frac{q_b}{\pi d_i L (t_b - t_{wx})} \quad (5)$$

And the BMF local Nusselt number can be obtained as:

$$\bar{Nu}_b(\text{exp}) = \frac{\bar{h}_b D_h}{k_b} \quad (6)$$

Where hydraulic diameter of annular space calculate as:

$$D_h = D_i - d_i \quad (7)$$

The experimental average heat transfer coefficient and Nusselt number of the BMF are computed from the following equation:

The BMF average heat transfer coefficient can be obtained as:

$$h_b = \frac{q_b}{(t_b - t_{wall})} \quad (8)$$

Then the BMF average Nusselt number can be obtained as:

$$Nu_b = \frac{h_b D_h}{k_b} \quad (9)$$

Similarly to the heat transfer coefficient, the friction factor of the BMF is calculated from:

$$f_b = \frac{2 D_h \Delta P_b}{L \rho_b u_b^2} \quad (10)$$

where (f_b) is the friction factor of the BMF, (ΔP_b) is the measured pressure drop of the BMF.

All BMFs employed in this study exhibit the power-law rheological behavior expressed by the following equation [28]:

$$\tau = m(\dot{\gamma})^n \quad (11)$$

In this work, the non-Newtonian fluids are based on a

power-law equation (Eq.11). Values of ($n < 1$) are shear-thinning fluids and with ($n > 1$) are shear-thickening fluids. For Newtonian fluids have ($n=1$). The shear stress is proportional with the fluid viscosity (μ) and shear strain($\dot{\gamma}$). For power-law shear-thinning fluids the wall shear rate is: [29]

$$\dot{\gamma}_{wall} = \frac{3n+1}{4n} \cdot \frac{8u_b}{D_h} \quad (12)$$

The effective viscosity at the wall shear rate is: [29]

$$\mu_{eff} = m(\dot{\gamma}_{wall})^{n-1} \quad (13)$$

For purely viscous non-Newtonian fluid, Wickramasinghe et al. [30] define a generalized Reynolds, Re_b for power law as follows

$$Re_b = \frac{\rho_b u_b^{2-n} D_h^n}{m} \cdot 8 \cdot \left(\frac{n}{6n+2} \right) \quad (14)$$

where u_b is the average velocity of the shear-thinning fluid, which may be related to the average velocity of a Newtonian fluid by:

$$u_b = \left(\frac{4n}{1+3n} \right) u_o$$

And modified Prandtl number is given by [31]:

$$Pr_b^* = \frac{c_p}{k_b} m \left(\frac{u_b}{D_h} \right)^{n-1} \quad (15)$$

The Graetz number is defined by:

$$Gz = \frac{\dot{m}_b c_p b}{k_b L} \quad (16)$$

The Péclet number is given by:

$$Pe_b = \frac{\rho_b c_p u_b D_h}{k_b} \quad (17)$$

5.2. Coolant Calculations

Using (Eq.2) to find the convection heat flux of nanofluid can be represented by:

$$q_{nf} = \frac{Q_{nf}}{A_i}$$

$$A_i = \pi d_o L$$

The nanofluid local heat transfer coefficient can be obtained as:

$$\bar{h}_b = \frac{q_{nf}}{\pi d_o L (t_b - t_{wx})} \quad (18)$$

And the nanofluid local Nusselt number can be obtained as:

$$\bar{Nu}_{nf} = \frac{\bar{h}_{nf} D_h}{k_{nf}} \quad (19)$$

Where hydraulic diameter of inner pipe calculate as: $D_h = d_i$

For Newtonian nanofluid, the Reynolds number is defined as:

$$Re_{nf} = \frac{\rho_{nf} u_{nf} D_h}{\mu_{nf}} \quad (20)$$

The Darcy friction factor (f) of the nanofluid flowing through inner pipe is defined as:

$$f_w = \frac{2 D_h \Delta P_w}{L \rho u_w^2} \quad (21)$$

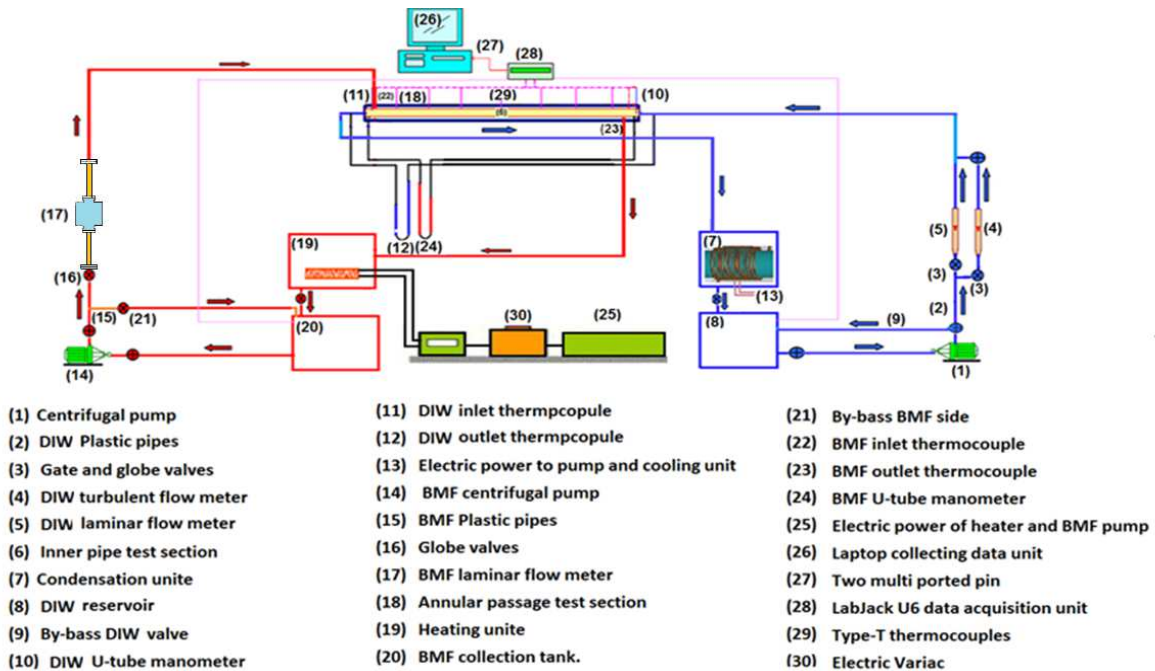


Figure 1. Schematic diagram of experimental rig used in present study.

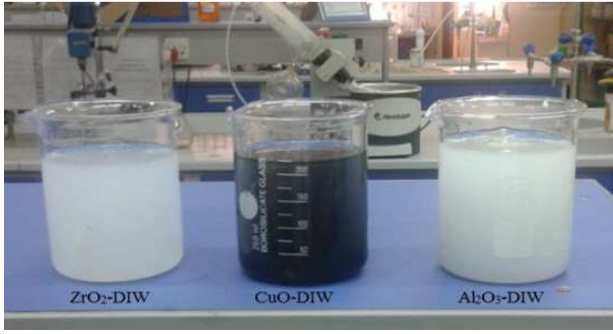


Figure 2. Samples of (ZrO_2 -DIW, CuO -DIW, γAl_2O_3 -DIW) nanofluids stability with time at $\phi=0.2\%$.

6. Results and Discussion

The experimental conditions used in this study are:

- (a) The flow rates of the laminar hot Newtonian BMF are (2, 3, 4 and 5 liter/min)
- (b) The flow rates of the laminar hot non-Newtonian BMF are (2.5, 3.5, 4.5 and 5.5 liter/min)
- (c) The temperatures of the hot BMF are (38, 40 and

42°C),

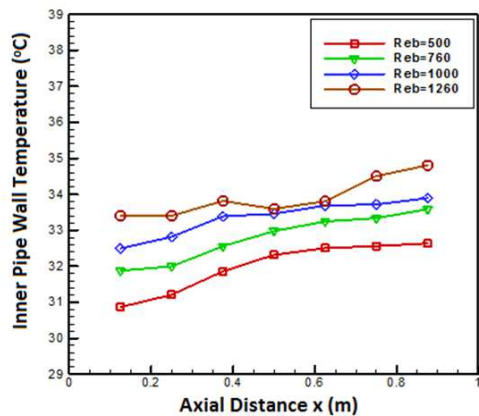
(d) The flow rates of the laminar cold nanofluid are (0.3, 0.5, 0.7 and 0.8 liter/min)

(e) The flow rates of the turbulent cold nanofluid are (2, 3, 4 and 5 liter/min)

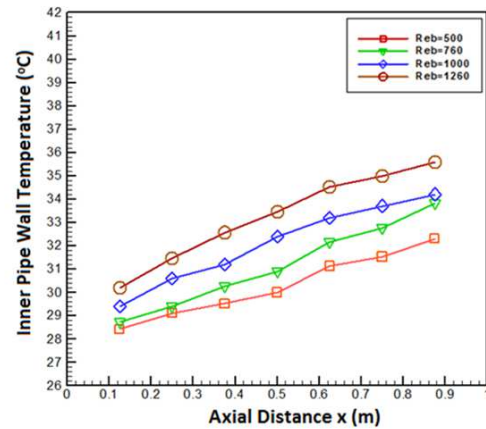
(f) The temperatures of the cold nanofluid are (18, 20 and 22°C).

6.1. Temperature Distribution

The variation curves of inner pipe wall temperatures (T_{wx}) have the general shape plotted in (Figure. 3a, b) in the case of using the nanofluid to cooling (BMF2 and BMF6) under the laminar condition. It shows that the (T_{wx}) increases gradually from (pipe inlet $x=0.0$ m), along the inner pipe until to attains a maximum value at (pipe exit $x=1.0$ m). (Figure. 4) shows the variation of (T_{wx}) for nanofluid laminar and turbulent flow to cool the Bovine blood ($H=35\%$) and BMF6 models it shows that the using BMF6 gives the nearest values of (T_{wx}). Due to approach between the non-Newtonian fluid behavior BMF6 and Bovine blood in the rheological behavior index (n) of the two fluids.

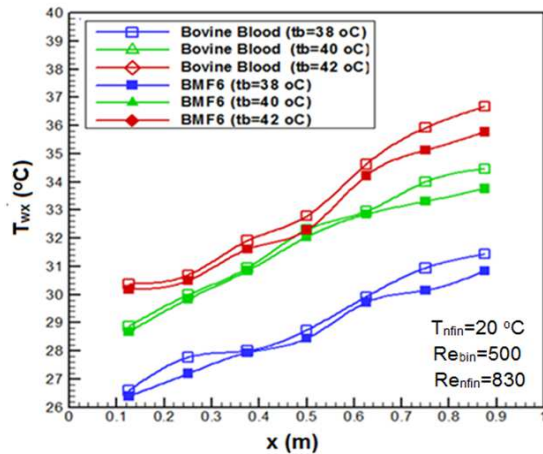


(a) BMF2

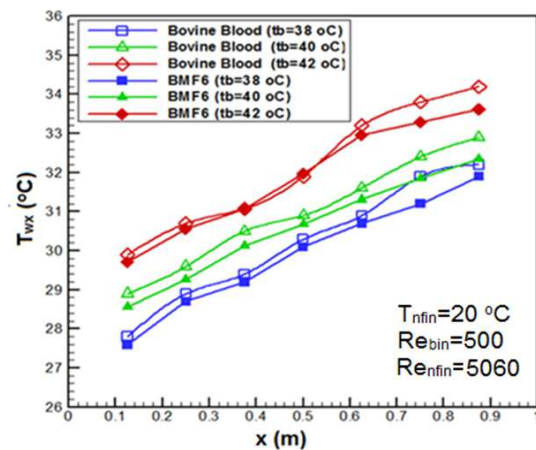


(b) BMF6

Figure 3. Effect of annular Reynolds number on the inner pipe wall temperatures (T_{wx}) for laminar DIW for cooling (BMF2 and BMF6) ($T_{nfin}=20^\circ C$, $T_{bin}=40^\circ C$ and $Re_{nfin}=830$).



(a) Laminar nanofluid



(b) Turbulent nanofluid

Figure 4. BMF inlet temperatures on inner pipe wall temperatures (T_{wx}) for cooling the Bovine blood and BMF6.

(Figure. 5) illustrates the effect of nanofluids types and concentrations on the experimental inner pipe wall temperature (T_{wx}) for cooling the (BMF2) for various nanofluid inlet temperatures. Show that the temperatures in the case of using (DIW, Al_2O_3 , CuO and ZrO_2 -DIW) at ($\phi=0.02$ vol. %) and can be show a good enhancement in decreasing (T_{wx}). where (Figure. 5. a) gives decreasing of (8.1%) when using Al_2O_3 , with using (Figure. 5c) CuO gives

(7.4%) and gives decreasing about (4.8%) when using ZrO_2 (Figure. 5e) instead of DIW. When increasing the concentration from ($\phi=0.02$ vol. %) Al_2O_3 (Figure. 5a) to ($\phi=0.2$ vol. %) Al_2O_3 (Figure. 5b) shows that the (T_{wx}) increasing about (13.5%) at ($t_{in}=18^\circ C$), this indicating the ability of Al_2O_3 -DIW fluid to extraction the heat from the inner wall and cooling the surface of the inner pipe by increasing the nanoparticles concentration.

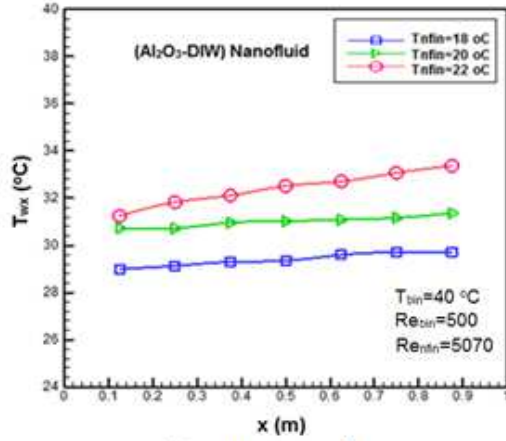
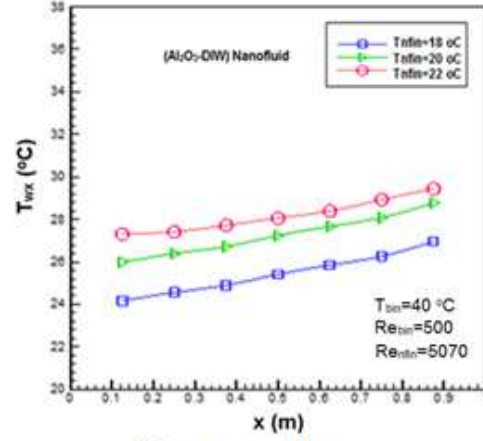
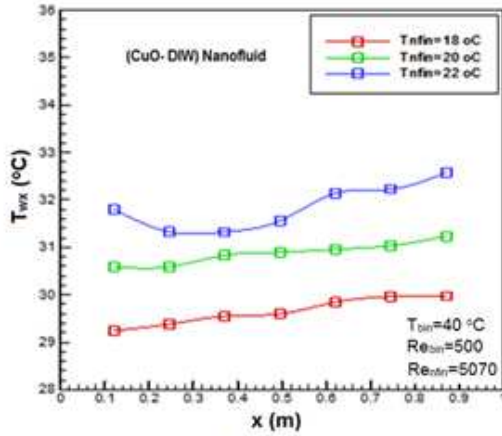
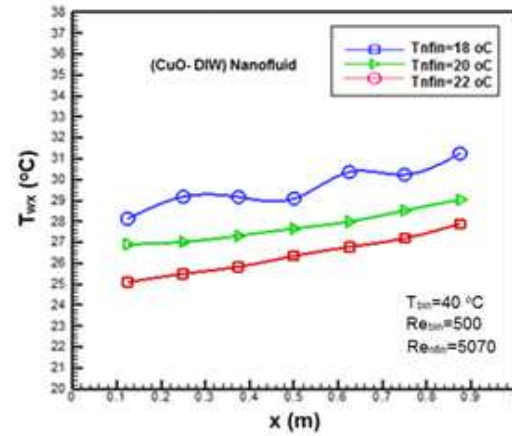
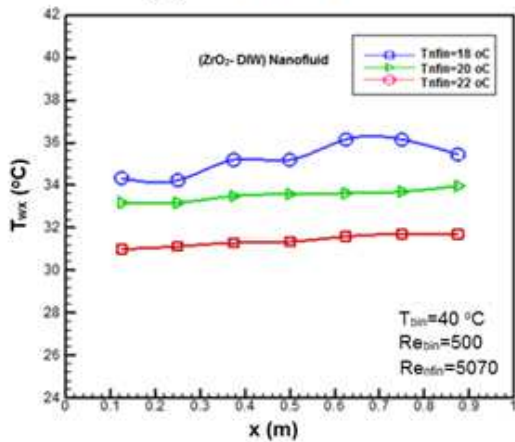
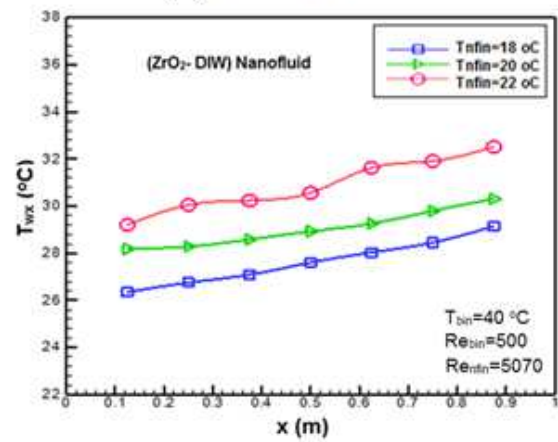
(a) $\phi=0.02$ vol. %(b) $\phi=0.2$ vol. %(c) $\phi=0.02$ vol. %(d) $\phi=0.2$ vol. %(e) $\phi=0.02$ vol. %(f) $\phi=0.2$ vol. %

Figure 5. Effect of nanofluids types and nanoparticles concentration on the inner pipe wall temperature (T_{wx}) to cooling (BMF2) for various nanofluid inlet temperatures.

The effect of the inner Reynolds number (nanofluid) can be found in (Figure. 6 a, b) for the case of using (Al_2O_3 -DIW) at concentration of the nanoparticles ($\phi=0.2$). It shows that the Reynolds number will be changed from case to another according to the types of the nanofluid and according to the concentration of the nanoparticles (ϕ) due to the differences in the thermo physical properties for various concentrations.

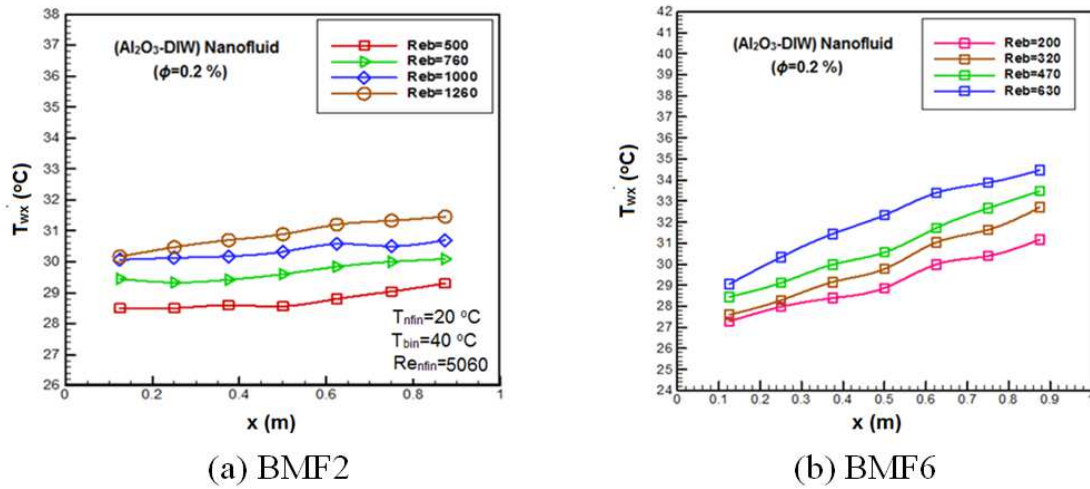


Figure 6. Effect of nanofluids types on the inner pipe wall temperature (T_{wx}) to cooling the (BMF2 and BMF6).

Comparison of using DIW and (Al_2O_3 -DIW) type on experimental (T_{wx}), (Figure. 7) shows that (T_{wx}) decreases significantly. This can be related to higher thermal conductivity and lower nanoparticle size of Al_2O_3 nanoparticle in Al_2O_3 -DIW nanofluid. This leads to high Brownian motion and increasing the conductance heat transfer between the inner pipe and the nanoparticles.

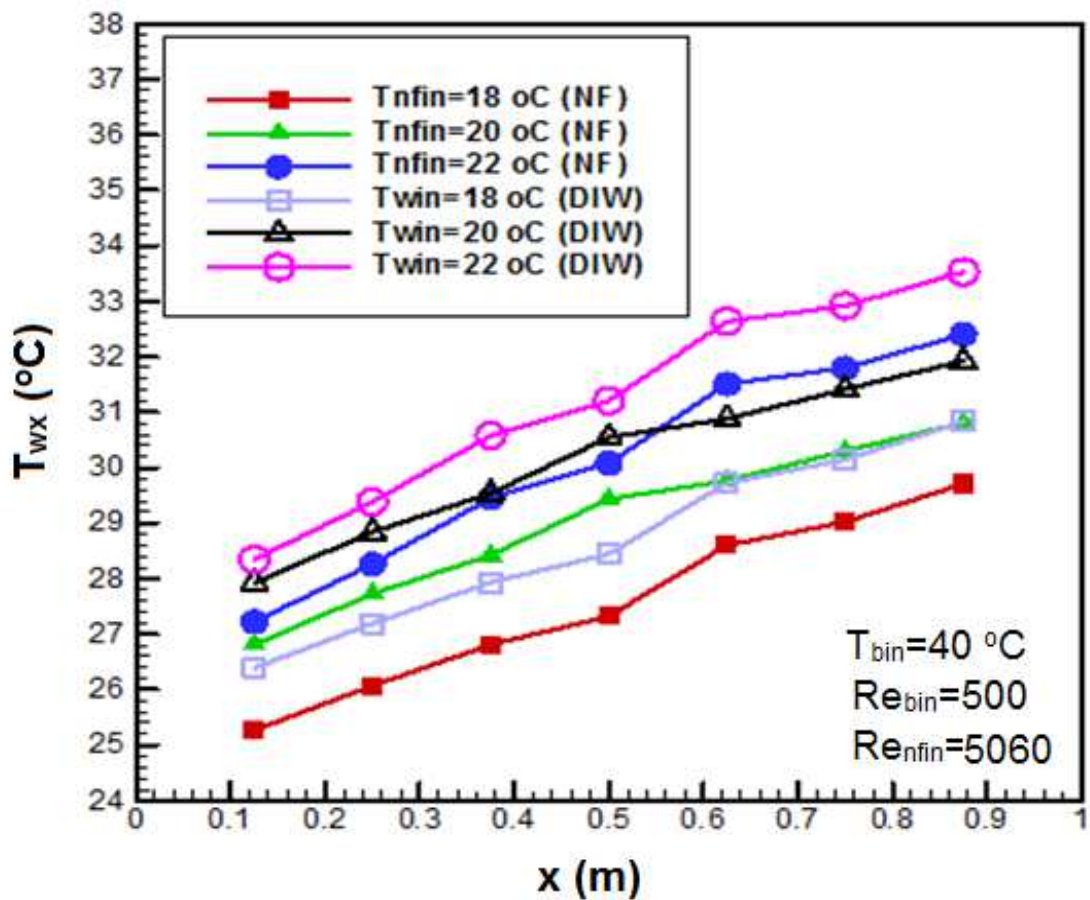


Figure 7. Effect of (Al_2O_3 -DIW- $\phi=0.2$ vol. %) type on the inner pipe wall temperature (T_{wx}) to cooling the (BMF2).

(Figure. 8 a, b) shows the effect of nanoparticles concentration in the case of using types of coolants (DIW, Al_2O_3 , CuO and ZrO_2) on the experimental (T_{wx}) to cool the (BMF2). Zero concentration of the nanoparticles ($\phi=0.0$) for (DIW), clearly show that increasing the concentration of the nanoparticles (ϕ) in the nanofluid decrease the (T_{wx}), in Al_2O_3 (Figure. 8 a). Increasing the concentration of the

nanoparticles ϕ (from 0.0 to 1.0 vol. %) causes a decrease in the (T_{wx}) by (8.1%). due to increasing of the thermal conductivity of the base fluid DIW for all types of nanofluid. (Figure. 8b) compares between coolant types (DIW, Al_2O_3 , CuO and ZrO_2). It shows that using Al_2O_3 gives the lowest (T_{wx}) and DIW gives the highest with decreasing percent of (12.1%).

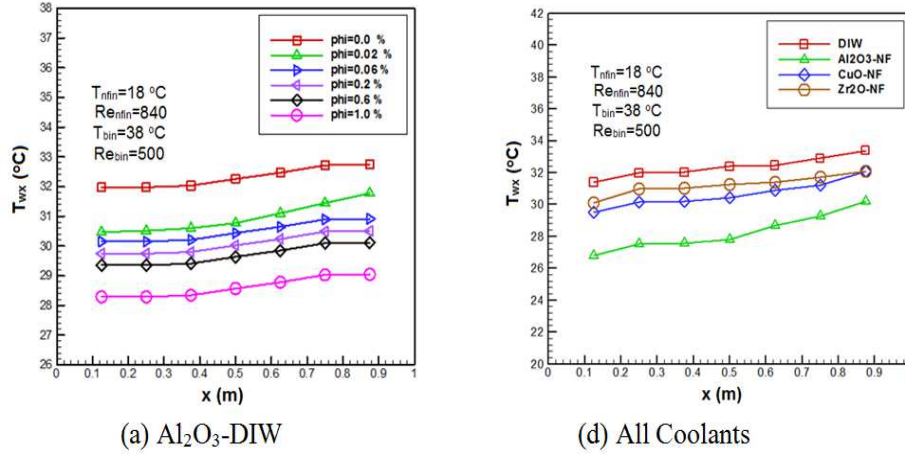


Figure 8. Effect of nanoparticles concentration of coolant types on the inner pipe wall temperature (T_{wx}), to cooling the (BMF2).

6.2. Convective Heat Transfer

Effect of using Bovine blood compared with BMF6 suggested in this study on the annular Nusselt number (Nu_b) with Gzatz number at the same experimental conditions showed in (Figure. 9). The results show the Bovine blood gives decreasing in (Nu_b) by (19.4%) compared with non-Newtonian BMF6 but gives maximum increasing of (Nu_b) if compared with Newtonian BMF2 by (14.6%) at ($Gz=500$).

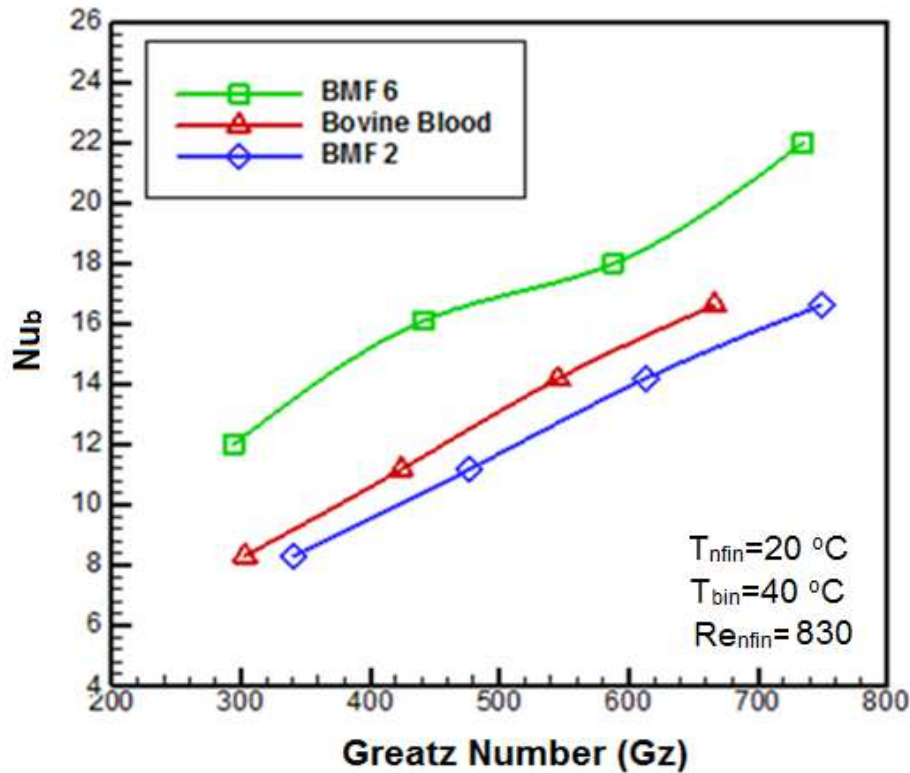
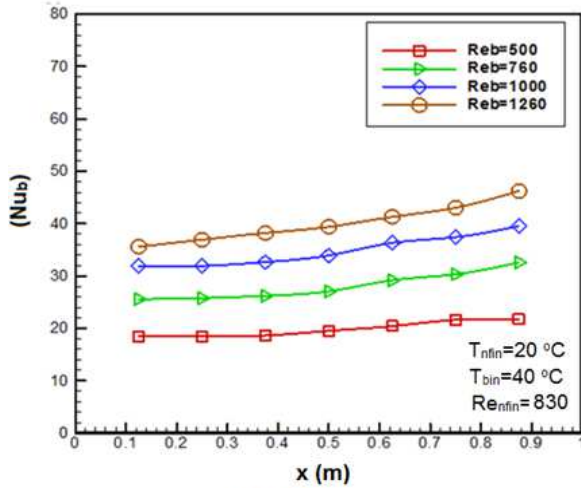


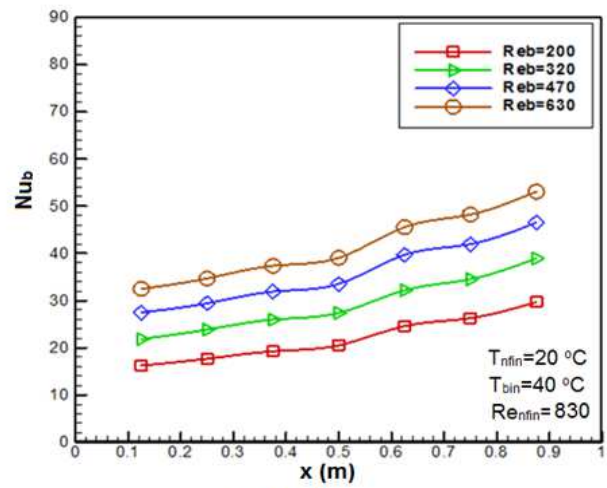
Figure 9. Effect of using Bovine blood and BMF6 types on variation of annular Nusselt number, with Gzatz number.

The effect of the annular Reynolds number of the BMF2 and BMF6 on the annular Nusselt number (Nu_b) is illustrated in (Figure. 10 a, b) for laminar DIW. The (Nu_b) began at high value at (pipe exit $x=1.0$ m) and dropped gradually forward to the (pipe inlet $x=0.0$ m) due to counter flow. And the overall behavior of (Nu_b) seems as straight line for the fully developing region in the test section. This shows that the annular Reynolds numbers different according to the BMF

models type because of the difference in the thermophysical properties and rheological behavior especially on the flow behavior index (n) between these fluids. It is observed that the (Nu_b) increases with annular Reynolds number. The Newtonian type (BMF1) in (Figure. 10a) gives maximum increasing of (51%) when increasing the Re_b from 500 to 1260.



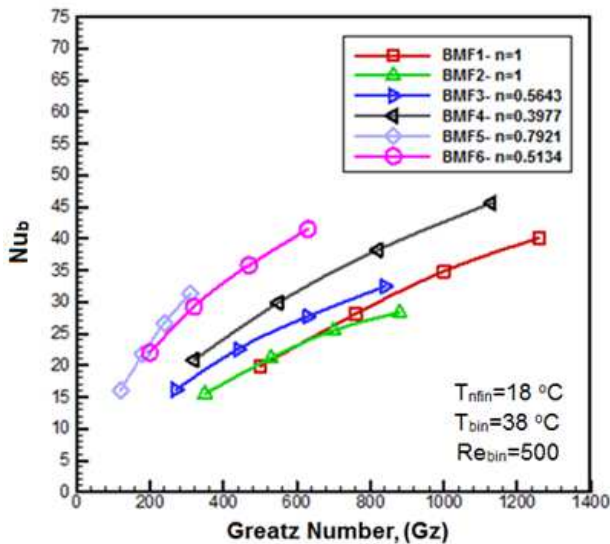
(a) BMF2



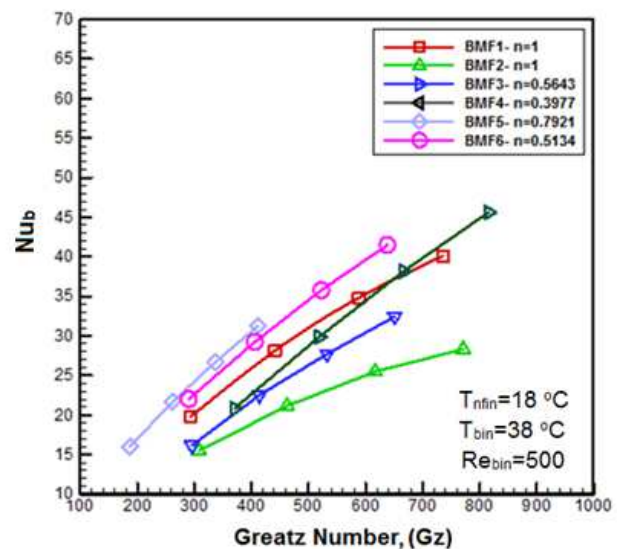
(b) BMF6

Figure 10. Effect of BMF types on the variation of annular Nusselt number, at various annular Reynolds number.

The types of BMF flow in the annulus, are given in (Figure. 11 a, b) for laminar and turbulent DIW flow conditions ($Re_w=830$ and 5070) with various Graetz number ($Gz=RePr$). The results show that the (Nu_b) increases by (51.6%) with increasing Gz from 500 to 1260 for using BMF1, and by (46.2%) when using BMF6 but the BMF4 gives the high (Nu_b).



(a) $Re_w=830$



(b) $Re_w=5070$

Figure 11. Effect of flow indices (n) and type of BMF on the annular Nusselt number (Nu_b).

(Figure. 12 a, b) presents the effect of inner nanofluid Reynolds number in the condition of turbulent flow, using (Al_2O_3 -DIW) at ($\phi=0.2$ %) as a coolant to cooling (BMF2 and BMF6). It is noted that the local inner Nusselt number (Nu_{in}) increased with increasing nanofluid Reynolds number by (82.4%) if Re_w increased from (5070 to 12670).

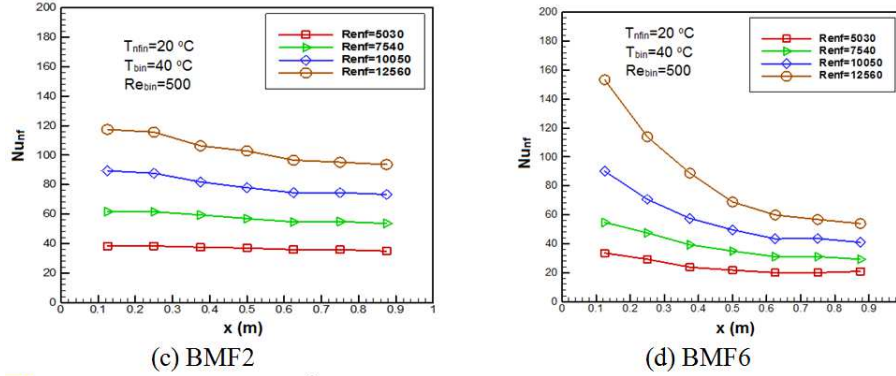


Figure 12. Effect of Inner Reynolds number on the inner Nusselt number, to cool a (BMF2 and BMF6).

The effect of increasing concentration (ϕ) on average inner Nusselt number with the inner Reynolds number shows in (Figure. 13 a, b). The laminar and turbulent flow conditions for DIW and (Al_2O_3 -DIW) to cool a (BMF2). It shows that the average inner Nusselt number increased with inner Reynolds number. And (Nu) increases with increasing the

concentrations by (53.3%) when increased the concentration from ($\phi=0.0$ to 1.0 vol. %) at $\text{Re}=1640$ in the laminar flow, and increased by (71.1%) in the turbulent flow at $\text{Re}=10050$. This is due to the enhancement in the thermal conductivity produced by adding the solid nanoparticles to the DIW.

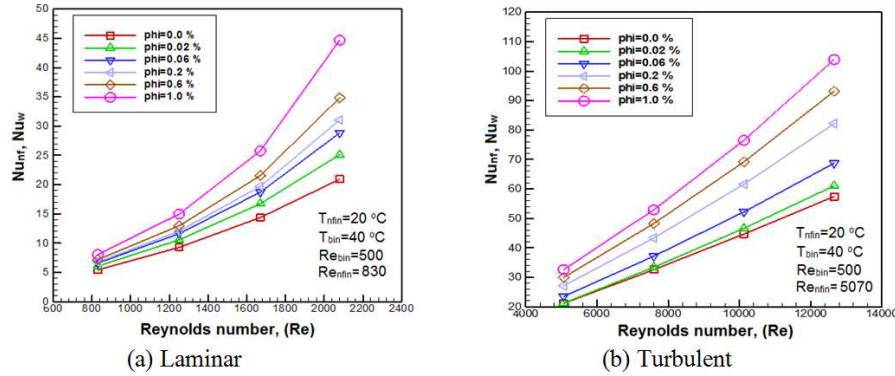


Figure 13. Effect of the nanoparticle concentration on the experimental variation of inner Nusselt number with the inner Reynolds number, of DIW and (Al_2O_3 -DIW) to cooling a (BMF2).

6.3. Friction Factor

Pressure drop results for the BMF models are presented in (Figure. 14 a, b). It shows the effect of the BMF types and flow index (n) of Newtonian and non-Newtonian (BMF) on the annular friction factor. It basically shows that the four non-Newtonian fluid BMF models have the highest values of friction factor as compared with the two Newtonian fluids BMF models due to increasing the fluid viscosity and rheological properties. (Figure. 14 a) shows that the (f_b) increases by (34.6%) at $\text{Re}=360$ between the BMF1 and BMF2.

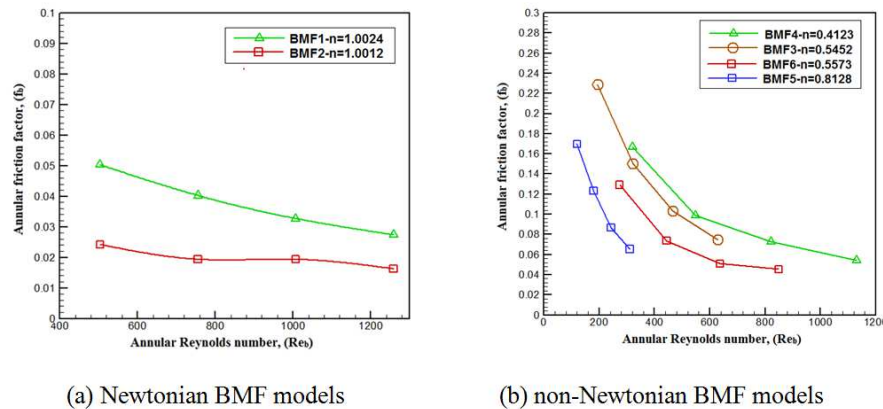


Figure 14. Effect of the BMF types and flow index (n) of Newtonian BMF on the annular friction factor with the annular Gz number.

(Figure. 15) shows the effect of using Bovine blood and BMF6 on the experimental annular friction factor with the annular Gertz number. It shows that the real bovine blood gives a maximum annular friction factor by (21.3%) compared with BMF6.

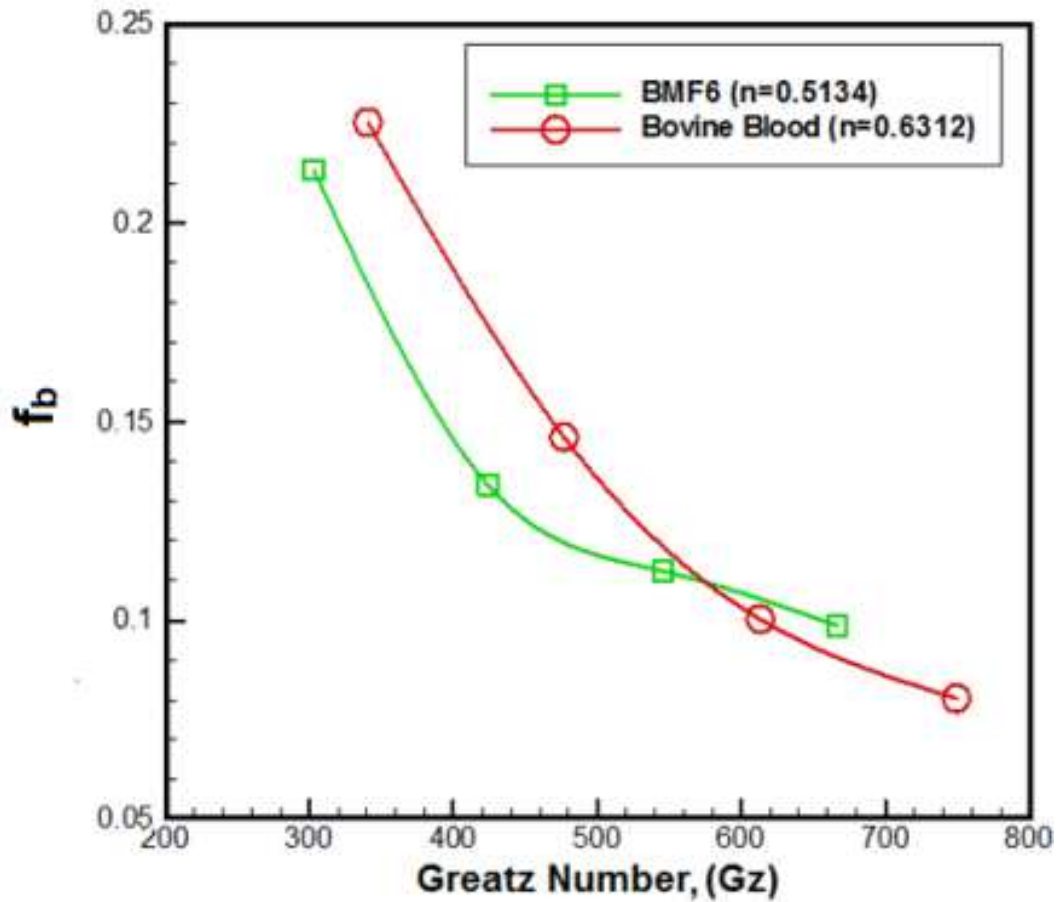


Figure 15. Effect of the Bovine blood and BMF6 on the annular friction factor.

The behavior of friction factor for the types of coolant at laminar and turbulent flow in (Figure. 16 a, b) shows that the inner friction factor decreases with increasing Reynolds number for all types. But when using (Al_2O_3 -DIW) gives the highest friction factor by (40.2%) for laminar condition at

$\text{Re}_{\text{nf}}=1630$ due to the smallest nanoparticles diameter of (20 nm) lead to increasing the nanofluid viscosity and then increased pressure drop. But (Al_2O_3 -DIW) shows the highest values for turbulent flow condition by (36.6%) at ($\text{Re}=10080$) as compared with the DIW.

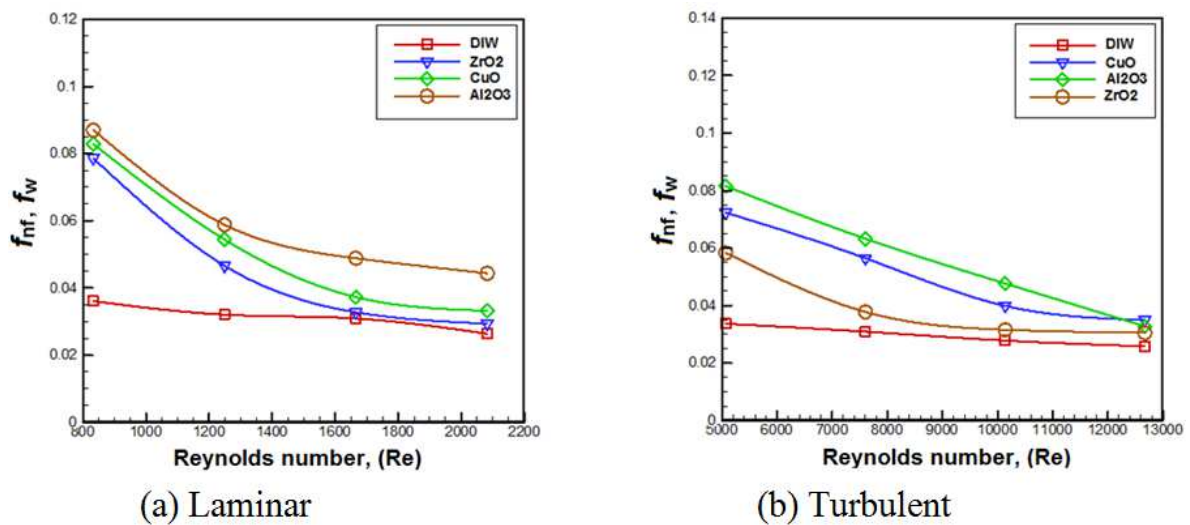


Figure 16. Effect of using three type of Nanofluid at ($\phi=0.2$) on the inner friction factor.

Effect of the concentration of (Al_2O_3 - DIW) on friction factor for laminar and turbulent flows presented in (Figure. 17 a, b). The inner friction factor for all nanofluids increases with increasing the nanoparticles concentrations by (33.2 %)

when ϕ increased (from 0.0 to 1.0 vol. %) for laminar $\text{Re}_w=1630$ and by about (36.3%) for turbulent $\text{Re}_w=10050$. The rise in friction factor is due to rise in viscosity of the nanofluids when the nanoparticles are adding to the DIW.

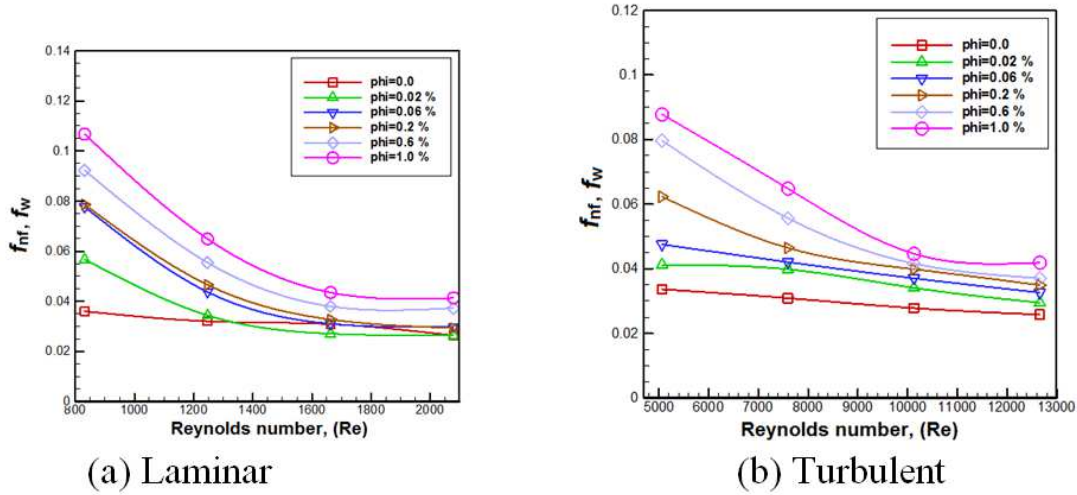


Figure 17. Effect of the nanoparticle concentration of (Al_2O_3 -DIW) on the inner friction factor.

6.4. Performance Evaluation Criterion (PEC)

Performance evaluation criterion: is defined as the ratio of heat transferred to the required pumping power in the BMF section [32]:

$$PEC = \frac{mcp (T_{out} - T_{in})}{v\Delta P} \quad (22)$$

(Figure. 18 a, b) shows the PEC was decreased with increasing inner Reynolds number due to increasing pressure drop across the inner pipe for all types of nanofluid at

concentration ($\phi=0.2$ vol. %). The DIW and ZrO_2 -DIW give low values and the CuO -DIW gives an increasing PEC by (52%) and Al_2O_3 -DIW gives increasing by (57%) for laminar condition of ($\text{Re}=1200$) than the using DIW. But for the case of turbulent flow, it can be observed that the value of PEC is very low compared with the laminar condition due to the higher value of pressure drop. The ZrO_2 -DIW gives an increasing in the PEC by (11%), for CuO -DIW by (34%) and for Al_2O_3 -DIW about (56%) at turbulent condition of ($\text{Re}=7500$).

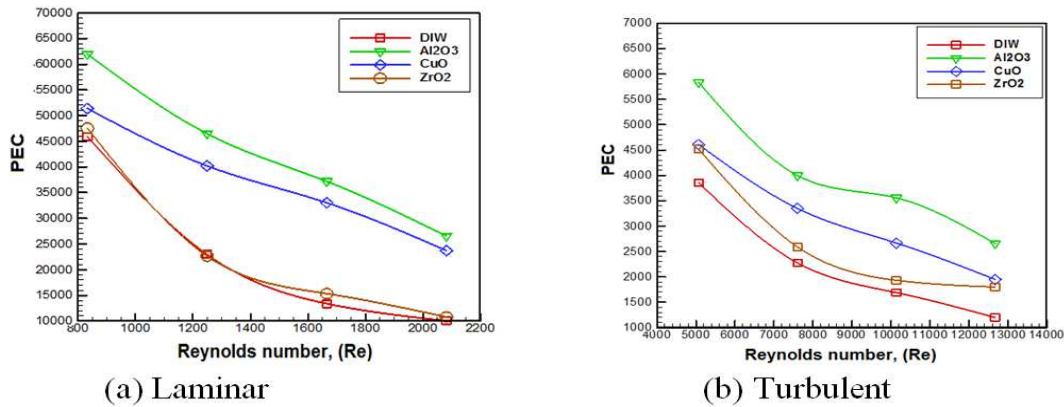


Figure 18. Effect nanofluid types at ($\phi=0.2$ vol. %) and DIW on (PEC) with the inner Reynolds number.

6.5. Validation Results with Proposed Correlations

To compared the experimental annular Nusselt number (Nu_b) for Newtonian and non-Newtonian BMF using (Figure. 19a, b) as comparison the experimental Results of (Nu_b) flow with the Newtonian and non-Newtonian Leveque Eq. [33] general equation (Eq. 23), and obtained on the acceptable agreements with deviation about (15.4%) for the

Newtonian BMF2 and about (9.7%) for the non-Newtonian BMF6.

$$\text{Nu}_b = 1.75 \text{Gz}^{1/3}, \quad (23)$$

$$\text{Nu}_b = 1.75 \Delta^{1/3} \text{Gz}^{1/3}$$

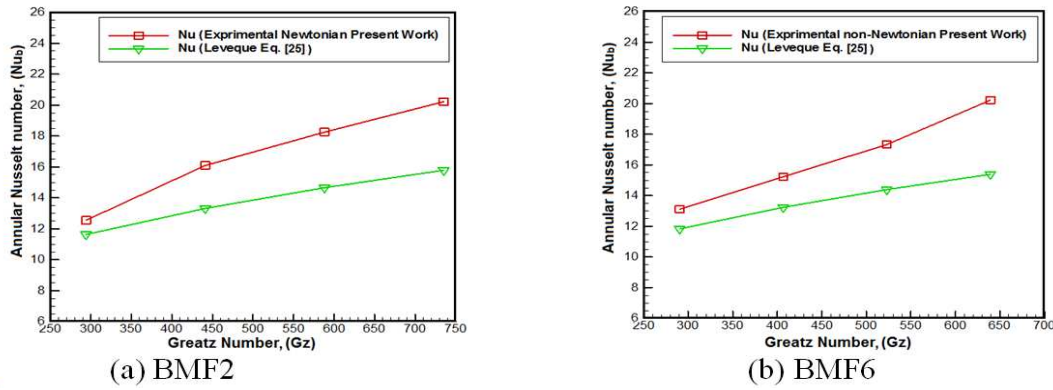


Figure 19. Comparison the experimental results of annular Nusselt number for Newtonian and non-Newtonian (BMF) flow with the Leveque [30] equation.

In general, Nusselt numbers and friction factor of the working fluids related with parameters listed in (Table.3).

Table 3. General form of the correlations.

Nanofluid	Laminar	Nu	$Nu_{nf} = f((RePrD/L)_{nf}^{a1}, \phi^{c1})$
		f	$f_{nf} = f(Re_{nf}^{a2}, \phi^{c2})$
	Turbulent	Nu	$Nu_{nf} = f(Re_{nf}^{a3}, P_{nf}^{b3}, \phi^{c3})$
		f	$f_{nf} = f(Re_{nf}^{a4}, \phi^{c4})$
BMF	Newtonian	Nu	$Nu_b = f(Gz_b^{a5}, \Delta^{c5})$ where $\Delta = 1 + 3n/4n$
		f	$f_b = f(Re_b^{a6}, \Delta^{c6})$
	non-Newtonian	Nu	$Nu_b = f(Gz_b^{a7})$
		f	$f_b = f(Re_b^{a8})$

The equation for predicting the heat transfer performance and friction factor of DIW, Al_2O_3 -DIW nanofluid and (BMF2, BMF6) was formed and is proposed in (Table. 4). The above equations are obtained by curve fitting all the experimental data for the (Al_2O_3 -DIW) nanofluids. Comparisons of the

experimental results with those calculated by the proposed correlation are shown in (Figure. 20). The results show good correspondence between the experimental values and the calculated values these equations, the data falls within ($\pm 22\%$) of the proposed equation.

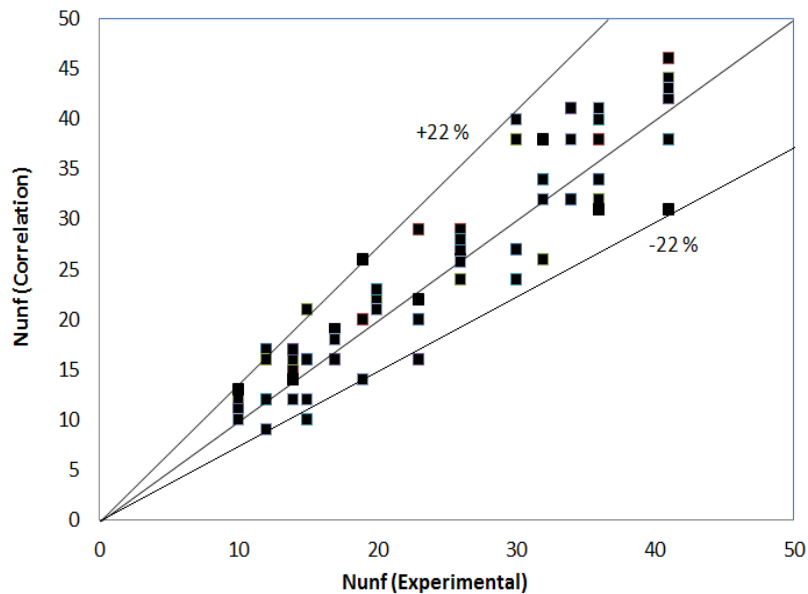


Figure 20. Plot comparing the correlation and experimental results of using Al_2O_3 -DIW to cooling BMF2.

Table 4. The equation for predicting the heat transfer and friction factor performance of DIW, Al_2O_3 nanofluid and Newtonian BMF2, and non-Newtonian BMF6 models.

Domain	Flow Condition	Parameter	Experimental Correlation	R ²
Al_2O_3 -DIW	Laminar	Nu	$Nu_{nf} = 1.623 \left(\frac{Re Pr D}{L} \right)^{0.8495} (\phi)^{0.03821}$	0.9965
		f	$f_{nf} = 74.222 (Re)^{-1} (\phi)^{0.02254}$	0.9852
	Turbulent	Nu	$Nu_{nf} = 0.0812 (Re)^{0.6895} (Pr)^{0.4844} (\phi)^{0.0681}$	0.9555
		f	$f_{nf} = 0.882 (Re)^{-0.3525} (\phi)^{0.0488}$	0.9552
(BMF)	Newtonian	Nu	$Nu_b = 1.2332 (Gz)^{0.4246}$	0.9226
		f	$f_b = 30.691 (Gz)^{-1.086}$	0.9435
	non-Newtonian	Nu	$Nu_b = 1.4221 (Gx)^{0.5426} (\Delta)^{0.4336}$	0.9662
		f	$f_b = 62.359 (Gz)^{-1.045} (\Delta)^{0.4552}$	0.9917

7. Conclusions

As a result of the experimental investigation which carried out to study forced convection heat transfer for the nanofluid flows in inner pipe and BMF flows in annular space of the double pipe system, the following conclusions can be made:

- The inner pipe wall temperature is affected by the extent of the local heat transfer which decreases as (a) increasing inner coolant Reynolds number (b) decreasing BMF Reynolds number (c) decreasing coolant inlet temperatures (d) decreasing BMF inlet temperatures, (e) using nanofluids of Al_2O_3 -DIW, CuO-DIW and ZrO_2 -DIW, (f) increasing the nanoparticles volume fraction. (g) Using high Re reduce the agglomeration of particles.
- The variation of BMF annular Nusselt number (Nu_b) for all cases may be affected by many factors, the Nu_b increases (a) with increases Re_b , (b) with decreasing flow behavior index (n) as the fluids changing from Newtonian to non-Newtonian fluids and increasing the shear thinning behavior.
- The variation of inner Nusselt number Nu_c increases (a)

by (22.2%) when the coolant inlet temperatures decreasing from 22 to 18°C, (b) increases with increasing Re_c , (c) by using the turbulent instead of laminar flow, (d) the high Nu_w obtained when using Al_2O_3 , gives a maximum enhancement by (82.4%) if Re_w increased from (5070 to 12670).

- The coolants inner friction factor (f_w and f_{nf}) decreasing with Re_c increasing for all cases, but using the (Al_2O_3 -DIW) will increase the friction factor values because its smallest nanoparticles diameter of (20 nm).
- The BMF inner friction factor f_b is decreasing with Gz increasing for all cases, but using the non-Newtonian BMF3, BMF4, BMF5 and BMF6 Types will increase the fraction factor values because the high viscosities and different rheological properties that Newtonian fluids BMF1 and BMF2. (f_b) increasing with decreasing the flow index (n).
- Bovine blood and BMF6 gives the nearest values of (T_{wx}), but the Bovine blood gives decreasing in (Nu_b) compared with BMF6 but gives maximum increasing of (Nu_b) if compared with Newtonian BMF2. And bovine blood gives a maximum friction factor compared with BMF6

Nomenclature

A	flow area, (m ²)	m	mass flow rate, (kg/s)
C_f	fanning friction factor	n	power-law consistency coefficient, (Pa. s ⁿ)
C_p	specific heat, (J/kg. K)	p	power law flow behaviour index, (–)
D_i	internal diameter of outer pipe, (m)	p	fluid static pressure, (Pa)
D_o	external diameter of outer pipe, (m)	Q	Heat transfer rate, (W)
D_h	hydraulic diameter, (m)	V	volumetric flow rate, (liter/min)
d_i	internal diameter of inner pipe, (m)	q	Convection heat flux, (W/m ²)
d_o	external diameter of inner pipe (m)	R^2	statistical value of linear regression
f	friction factor=Darcy friction factor	T_{wx}	local inner pipe wall temperature, (°C)
H	haematocrit, (%)	T_{wall}	average inner pipe wall temperature, (°C)
h	heat transfer coefficient, (W/ m ² . K)	u_o	bulk axial velocity, (m/s)
k	thermal conductivity, (W/m. K)	$\Delta p/L$	pressure drop per unit length, (Pa/m)
L	axial length, (m)	x	axial distance along pipe, (m)
Greek letters		Subscripts	
$\dot{\gamma}$	shear rate, (s ⁻¹)	ave	average
μ	dynamic viscosity, (Pa. s)	b	blood or BMF

μ_{eff}	effective viscosity, (Pa. s)
ν	kinematic viscosity, m^2/s)
τ	shear stress, (N/m^2)
ρ	density, (kg/m^3)
ϕ	nanoparticles concentration, (%)

w	water
i	inner
o	outer
in	inlet
out	outlet
c	coolant

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